

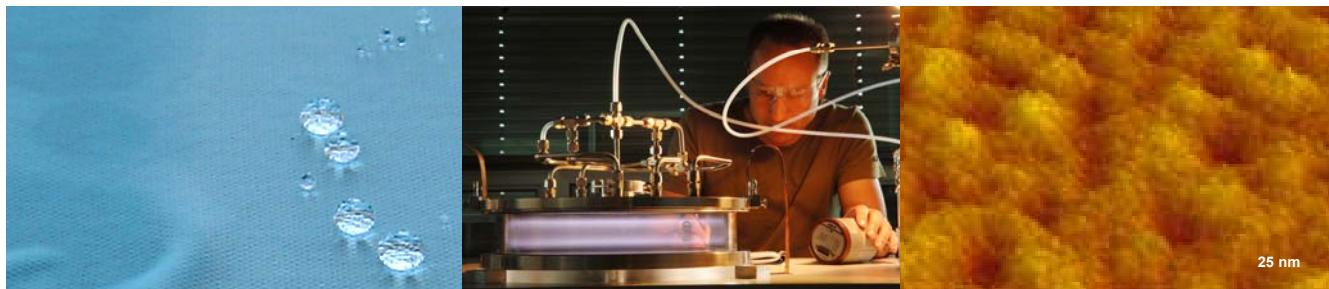


18th Int. Sym. on Plasma Chemistry  
August 26-31, 2007, Kyoto, Japan



Materials Science & Technology

# Control of Plasma Polymerization Processes



Dr. Dirk Hegemann  
Empa, St.Gallen, Advanced Fibers  
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## Empa, Swiss Materials Science & Technology

Member of ETH board in Switzerland  
865 employees at three sites  
→ R&D for (international) SMEs



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# Empa Laboratory

## Advanced Fibers

### ■ Fiber and Textile Chemistry

- finishing, wet-chemical treatment



### ■ Fiber Development

- bi-component fiber spinning device



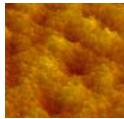
### ■ Plasma-modified Surfaces

- cleaning, activation, deposition



## Outline

### Control of Plasma Polymerization Processes



#### ■ Plasma polymerization

#### ■ Influence of

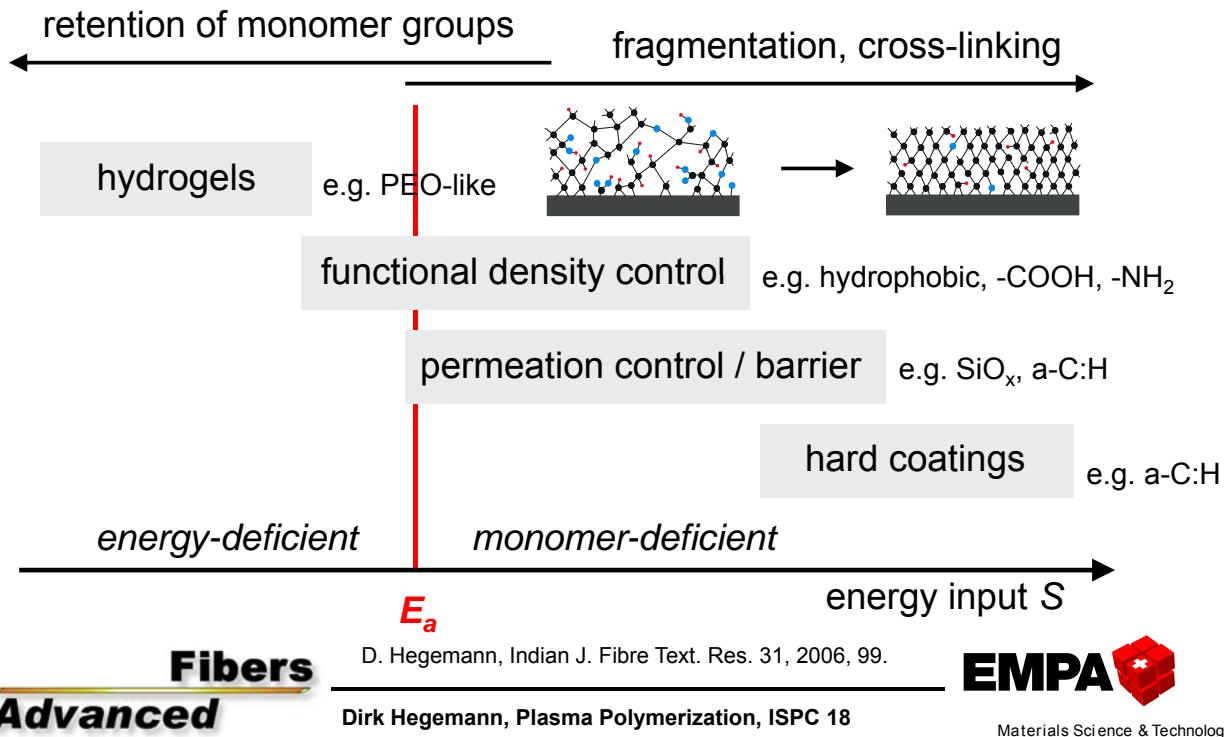
- reactor geometry
- plasma expansion
- pressure
- monomers
- carrier / reactive gas

#### ■ Nanoporous coatings

#### ■ Scale-up

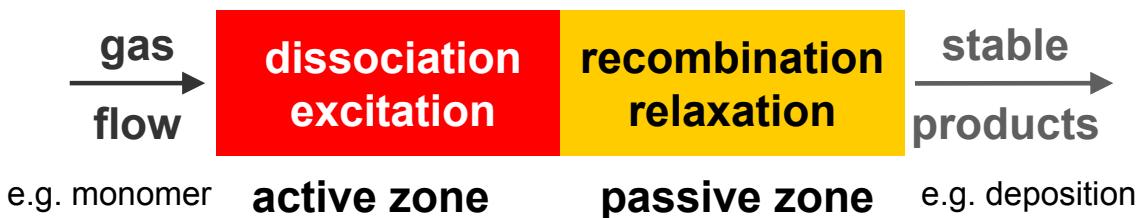
# Plasma Polymerization

## Different regimes



## Macroscopic Kinetics

### Concept of chemical quasi-equilibria related to plasma



**Macroscopic kinetics:  
(Becker formula)**

$$S = \frac{W\tau_{act}}{pV_{act}} \propto \frac{W}{F}$$
$$\tau_{act} = \frac{pV_{act}}{p_0 F}$$

The similarity parameter  $S$  represents the energy invested per particle of the gas mixture during the flow through the active plasma zone.

H.-E. Wagner, in: Low Temperature Plasma Physics, ed. Hippler et al., Wiley-VCH, 2001, p. 305.

A. Rutscher, H.-E. Wagner, Plasma Sources Sci. Technol. 2, 1993, 279.

# Plasma Polymerization

## Evaluation of deposition rates

For radical-dominated discharges the reaction parameter power input per gas flow  $W/F$  within the active plasma zone determines the mass deposition rate  $R_m$

$$\frac{R_m}{F} = G \exp\left(-\frac{E_a}{W/F}\right)$$

in [g/cm<sup>5</sup>]  
deposited mass from (per)  
plasma volume and per area

$E_a$ : (apparent) activation energy

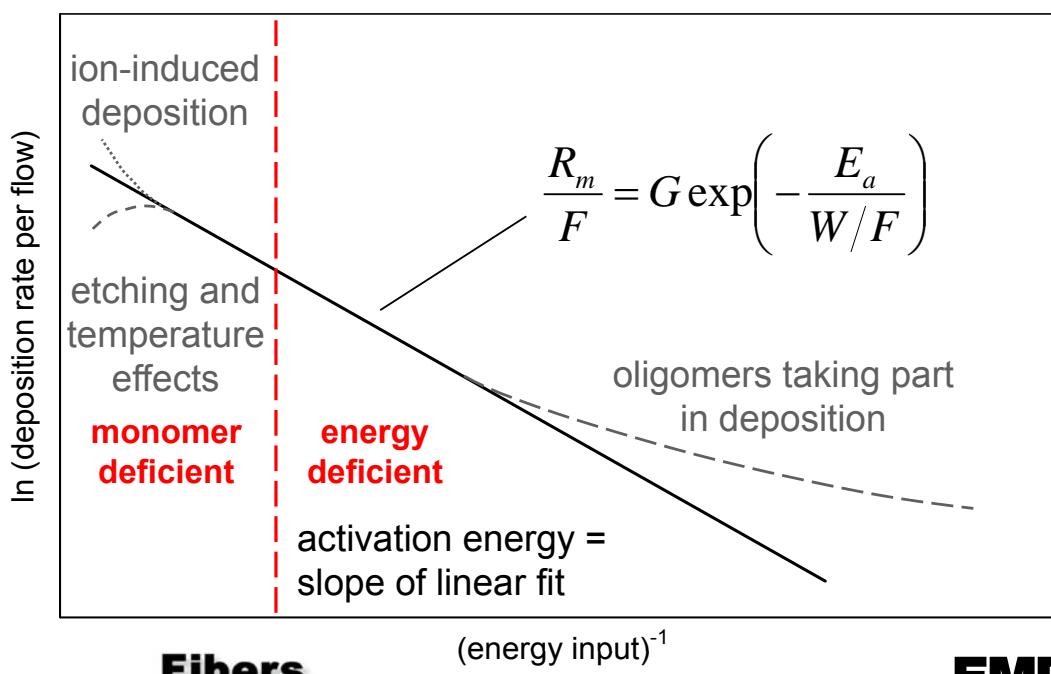
G: geometrical factor

Y.S. Yeh, I.N. Shyy, H. Yasuda, J. Appl. Polym. Sci.: Appl. Polym. Symp. 42, 1988, 1.

D. Hegemann, H. Brunner, C. Oehr, Plasmas Polym. 6, 2001, 221.

# Plasma Polymerization

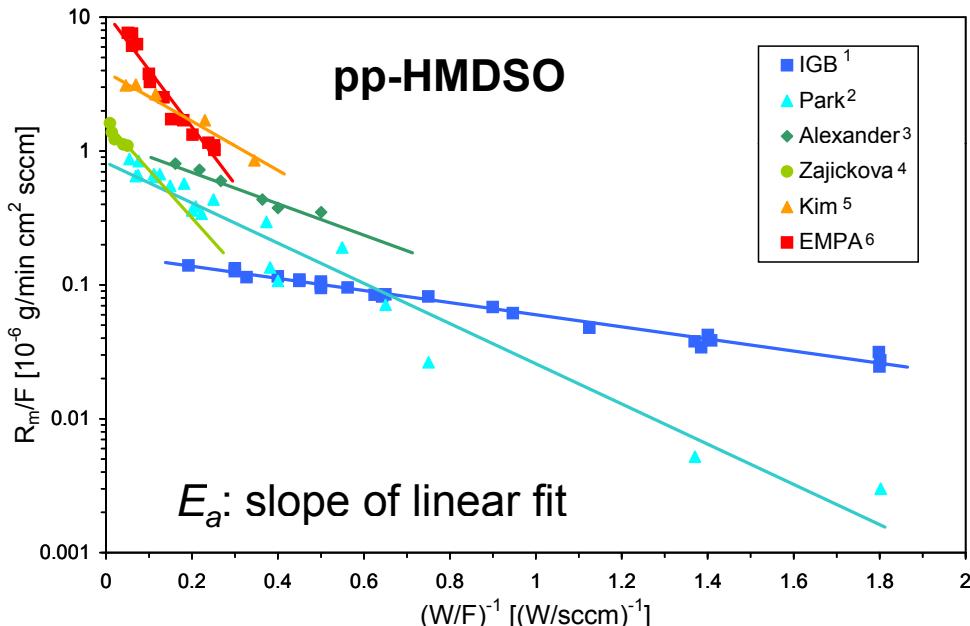
## Evaluation of deposition rates



D. Hegemann,  
M.M. Hossain,  
Plasma Process.  
Polym. 2, 2005,  
554.

# Evaluation of Deposition Rates

## Deposited mass for different reactor geometries



<sup>1</sup> Hegemann et al., Plasma Polym. 6, 2001, 221.

<sup>2</sup> Park, N. Kim, J. Appl. Polym. Sci.: Appl. Polym. Symp. 46, 1990, 91.

<sup>3</sup> Alexander et al., Plasma Polym. 2, 1997, 277.

<sup>4</sup> Zajickova et al., Proc. ISPC 14, 1999, 1439.

<sup>5</sup> M.T. Kim, Thin Solid Films 311, 1997, 157.

<sup>6</sup> Hegemann et al., J Vac Sci Technol A23, 2005, 5.

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## Influence of Reactor Geometry

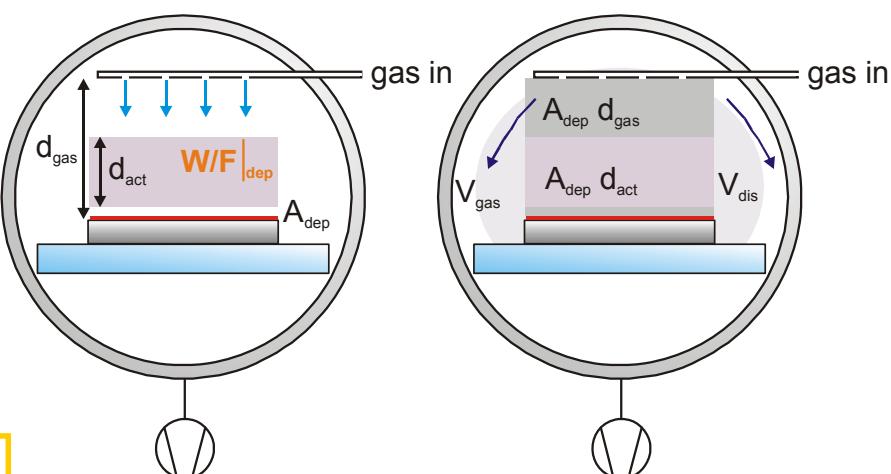
### Plasma deposition in a reaction vessel

$$S = \frac{W}{F} \Big|_{dep}$$

$$W|_{dep} = W \frac{A_{dep} d_{act}}{V_{dis}}$$

$$F|_{dep} = F \frac{A_{dep} d_{gas}}{V_{gas}}$$

$$S = \frac{W}{F} \frac{d_{act}}{d_{gas}} \frac{V_{gas}}{V_{dis}}$$



Similarity parameter is related to power and flow that contribute to film deposition.

D. Hegemann et al., Thin Solid Films 491, 2005, 96; Surf. Coat. Technol. 200, 2005, 458.

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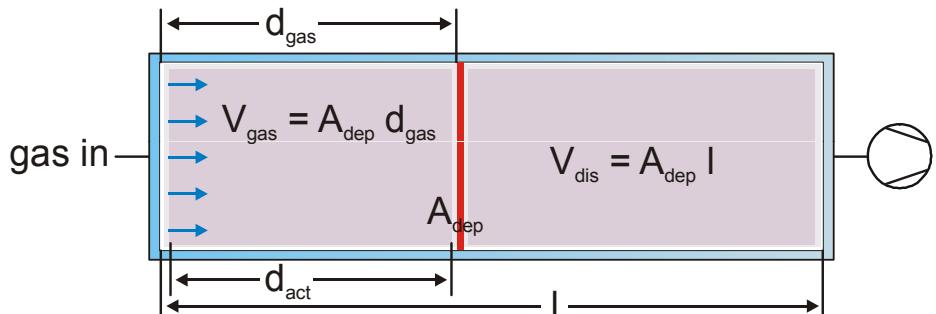
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# Influence of Reactor Geometry

## Tubular set-up

$$S = \frac{W}{F} \frac{d_{act}}{l}$$



$$S = \frac{W}{p} \frac{\tau_{act}}{V_{dis}} \quad \tau = \frac{V}{F} \frac{p}{p_0} ; T = \text{const.}$$

Similarity parameter changes with position of substrate within the discharge.  
→ Fragmentation increases with distance and residence time

J.M. Kelly, R.D. Short, M.R. Alexander, Polymer 44, 2003, 3173.

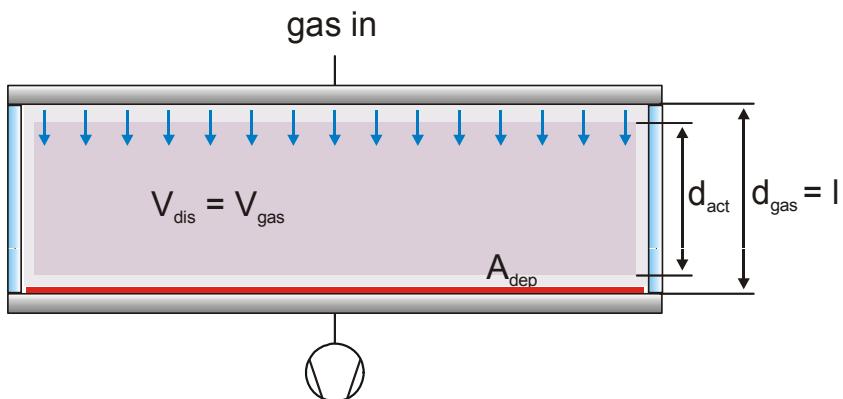
# Influence of Reactor Geometry

## Symmetric plane parallel set-up

$$S = \frac{W}{F} \frac{d_{act}}{l}$$

$$l = d_{act} + 2d_{sh}$$

$$S = \frac{W}{F} \left( 1 - 2 \frac{d_{sh}}{l} \right)$$



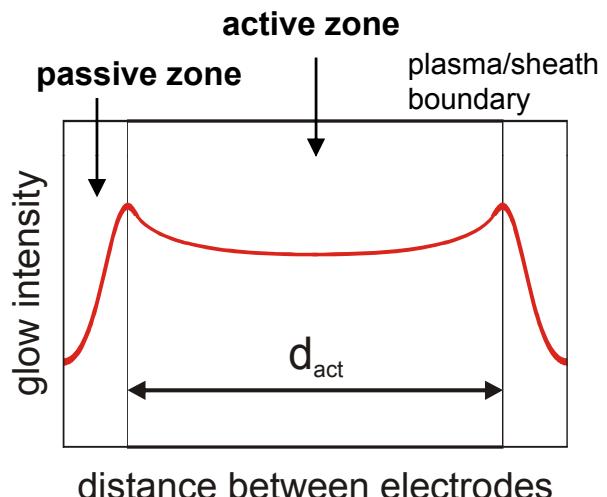
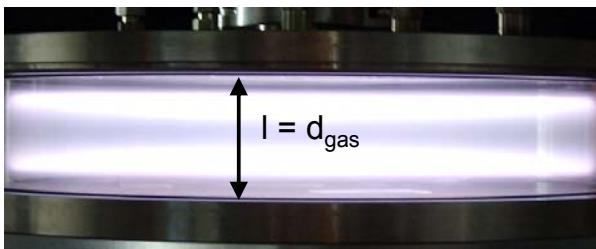
Similarity parameter increases with electrode distance.

D. Hegemann, H. Brunner, C. Oehr, Surf. Coat. Technol. 142-144, 2001, 849.

V. Sciarratta, D. Hegemann, M. Müller, U. Vohrer, C. Oehr, in: Plasma Processes and Polymers, Wiley-VCH, 2005, p. 39.

# Symmetric Reactor

## Plasma length $d_{act}$



- well defined geometrical conditions
- known gas flow (vertical flow)
- known power adsorption

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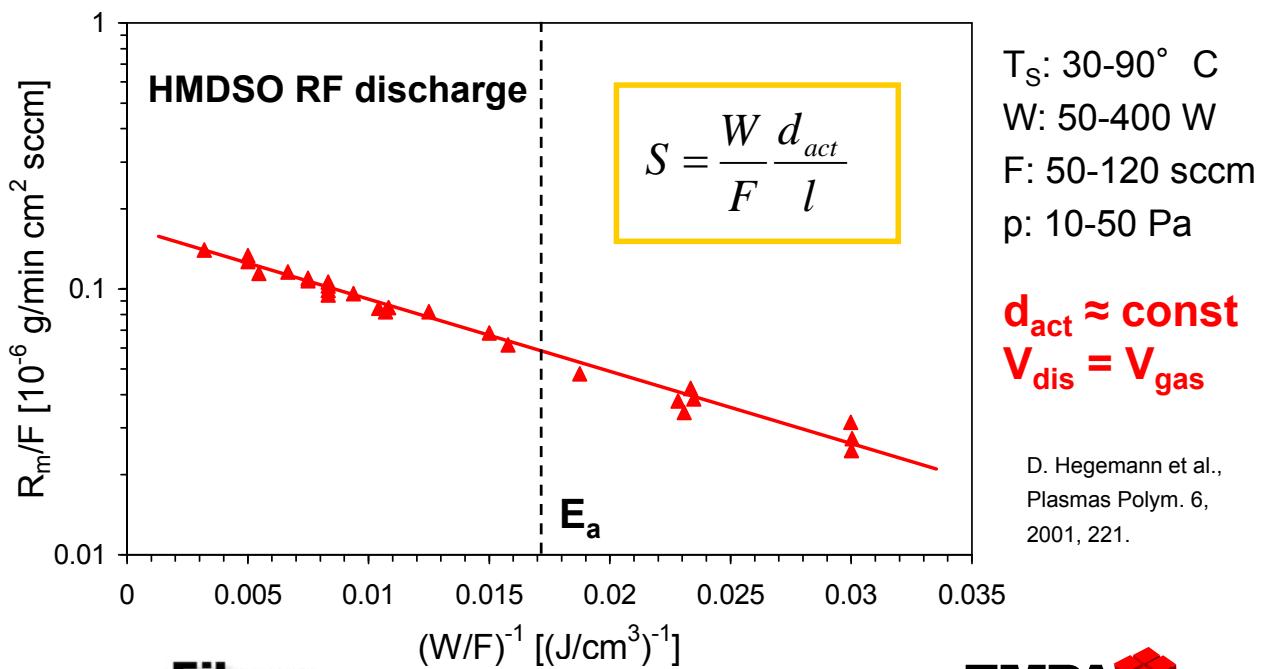
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# Symmetric Reactor

## Variation of temperature, power, flow, and pressure



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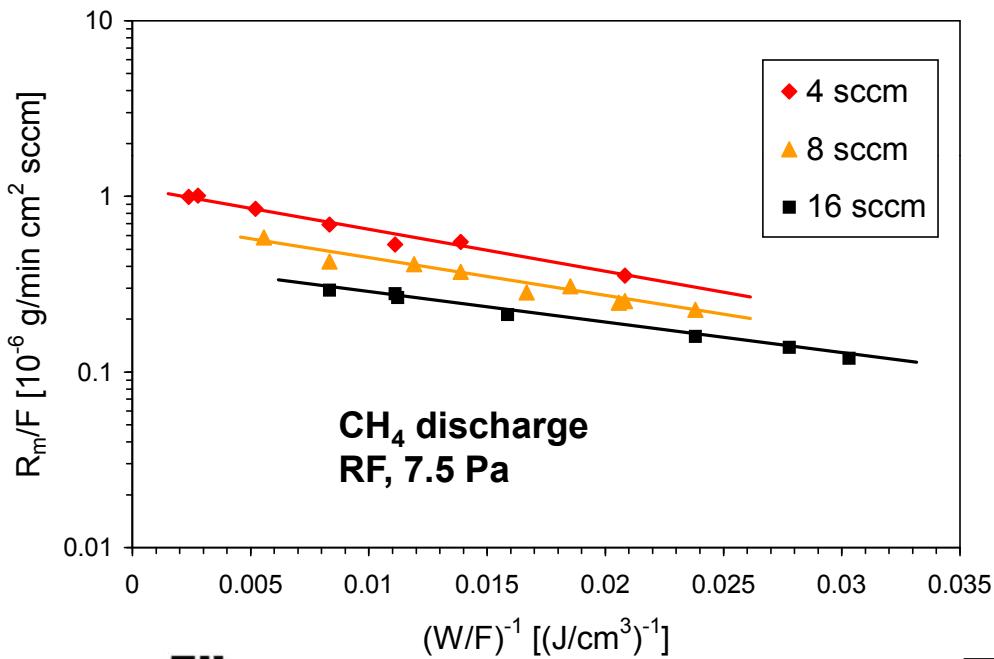
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# Influence of Plasma Expansion

## Plasma polymerization within asymmetric discharges



Different activation energies (slopes) were obtained for different gas flows.

D. Hegemann et al.,  
Thin Solid Films  
491, 2005, 96.

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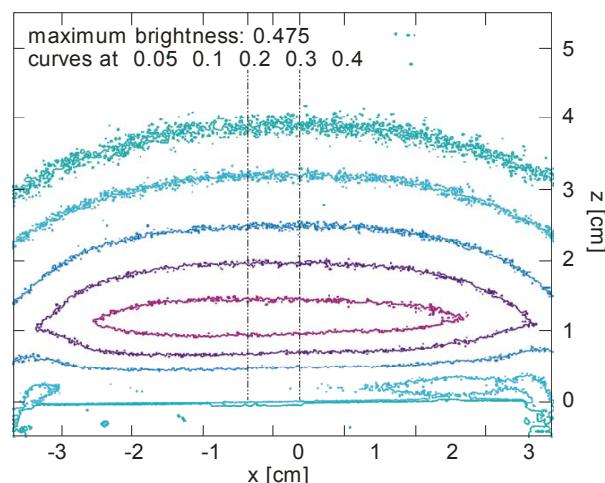
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# Influence of Plasma Expansion

## Light distribution of plasma in front of RF electrode



$\text{CH}_4$  discharge  
RF, 7.5 Pa



D. Hegemann et al., Thin Solid Films 491, 2005, 96.

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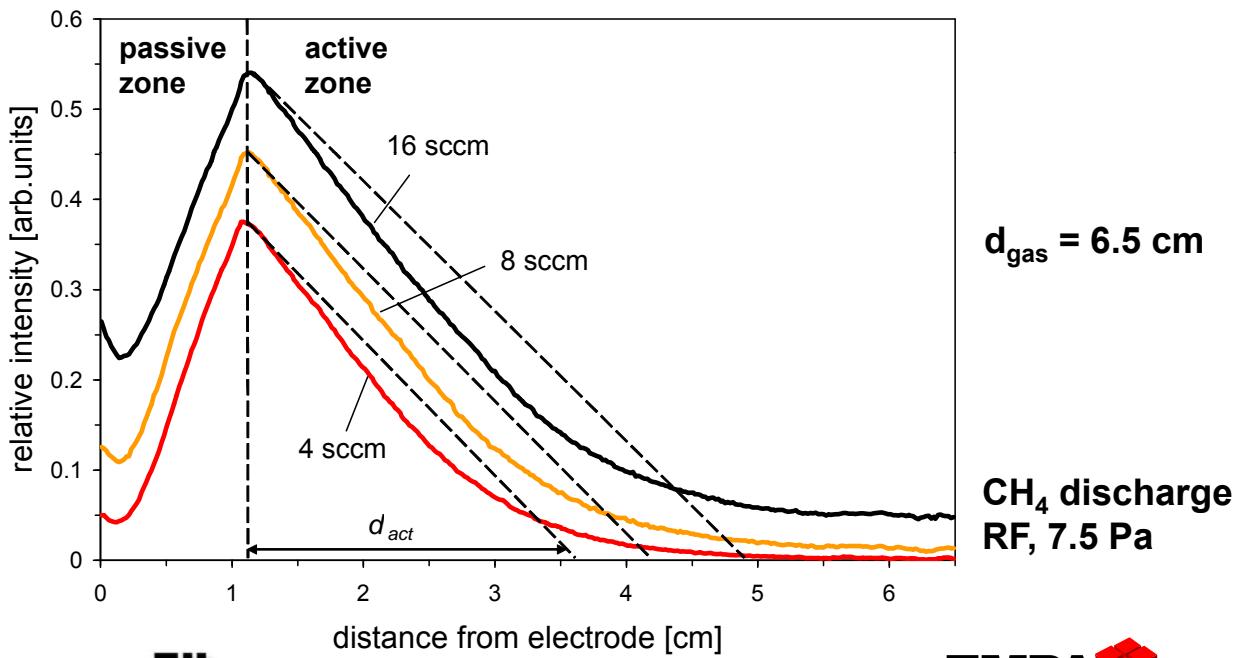
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# Influence of Plasma Expansion

## Light distribution of plasma in front of RF electrode



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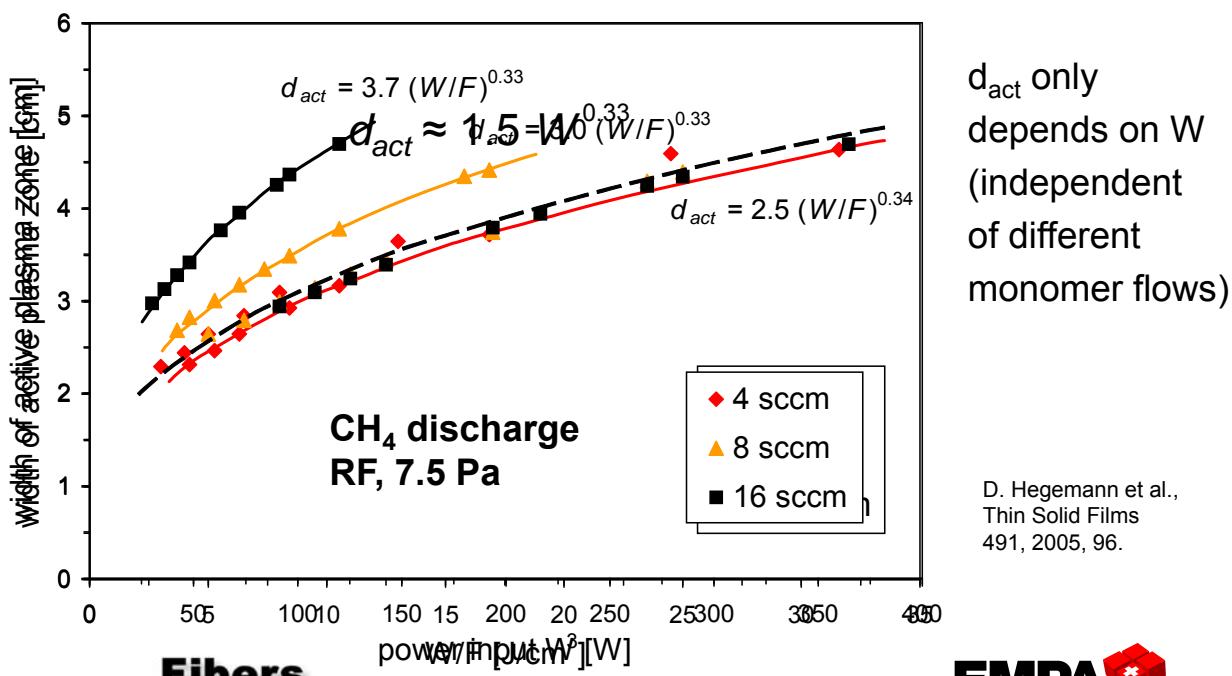
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# Influence of Plasma Expansion

## Expanding plasma zone depending on power and flow



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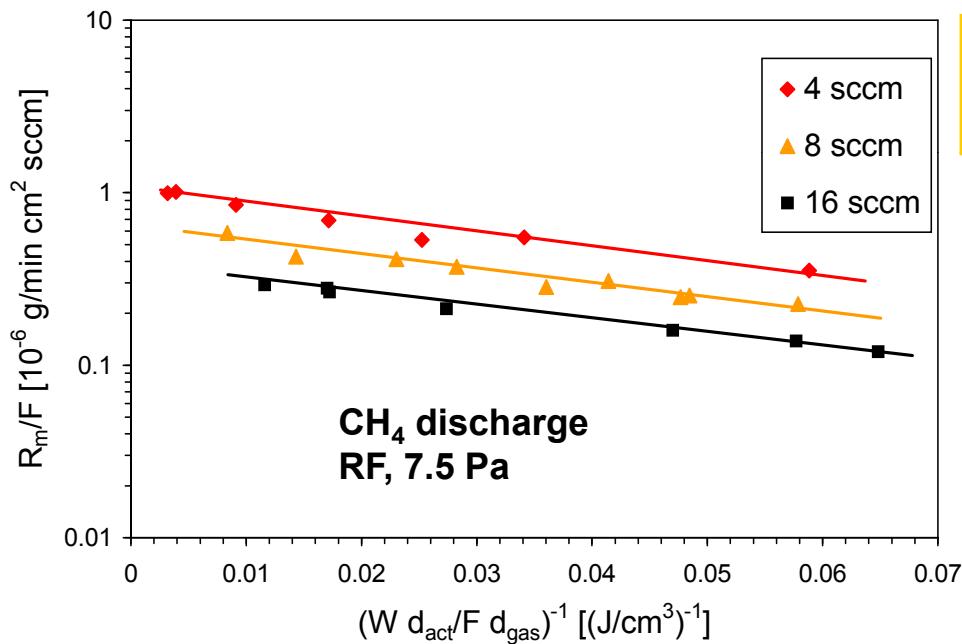
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# Influence of Plasma Expansion

## Consideration of similarity factor

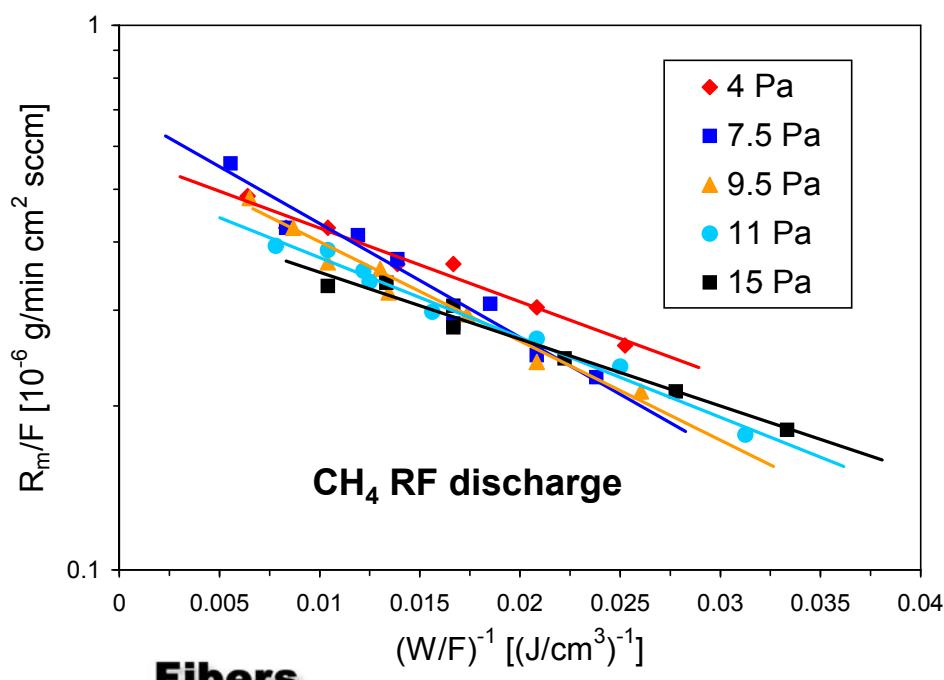


$$S = \frac{W}{F} \frac{d_{act}}{d_{gas}} \frac{V_{gas}}{V_{dis}}$$

Introduction of similarity factor yield same activation energy.

# Influence of Pressure

## Plasma polymerization within asymmetric discharges

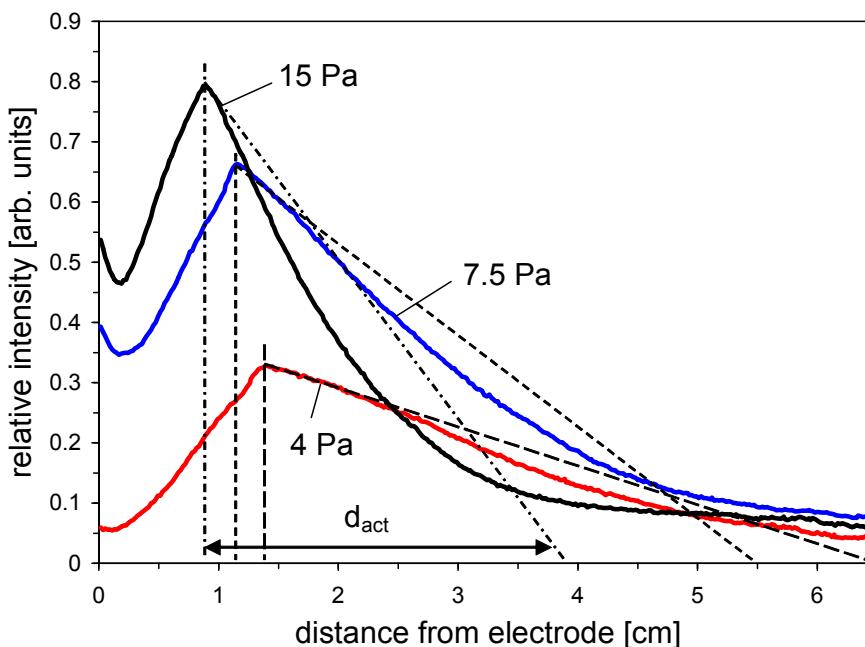


Different activation energies (slopes) were obtained for different pressures.

D. Hegemann,  
Thin Solid Films  
515, 2006, 2173.

# Influence of Pressure

## Light distribution of plasma in front of RF electrode



$d_{\text{gas}} = 6.5 \text{ cm}$

CH<sub>4</sub> RF discharge

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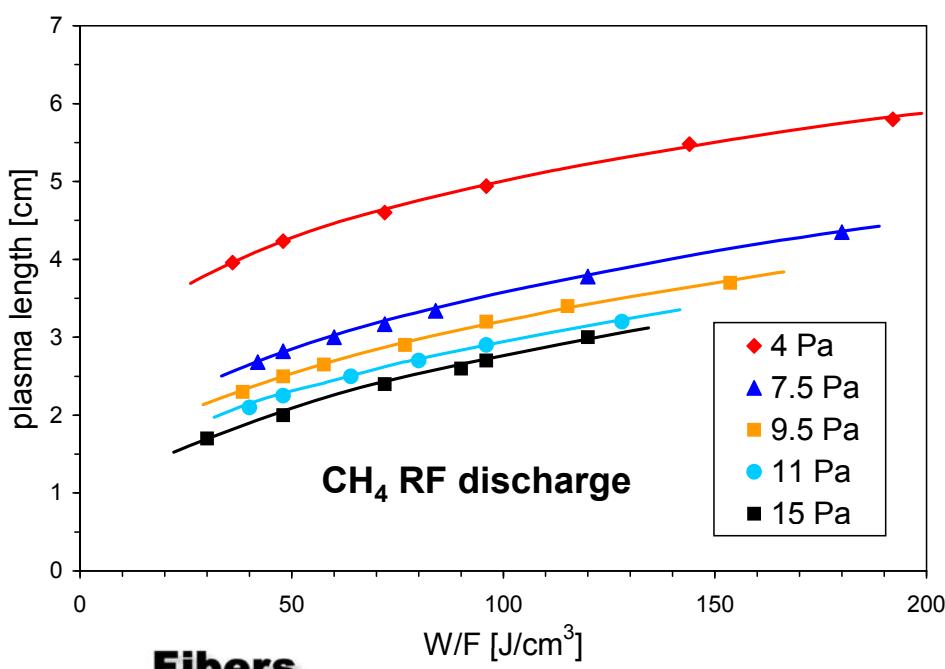
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# Influence of Pressure

## Expanding plasma zone depending on energy input



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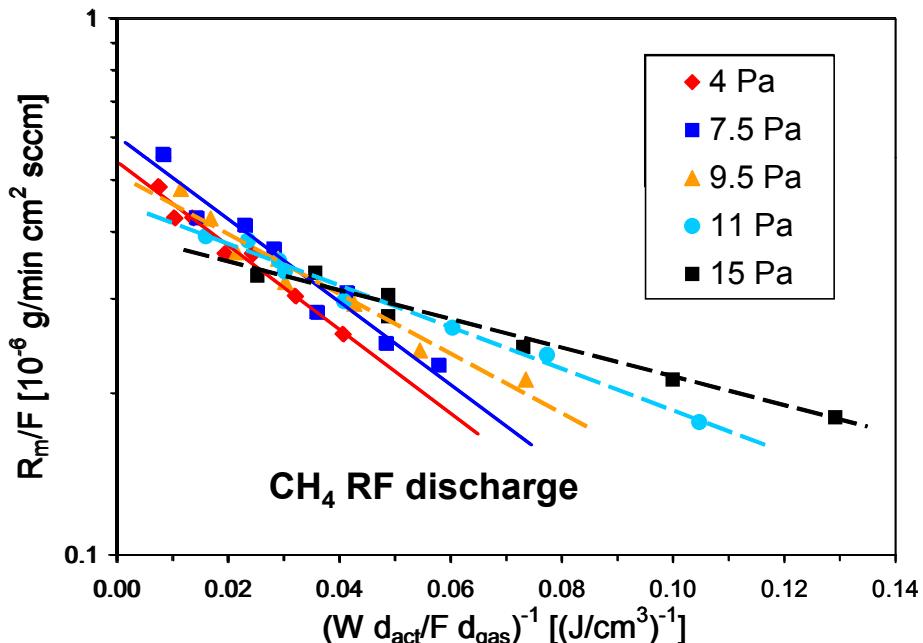
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# Influence of Pressure

## Consideration of similarity factor



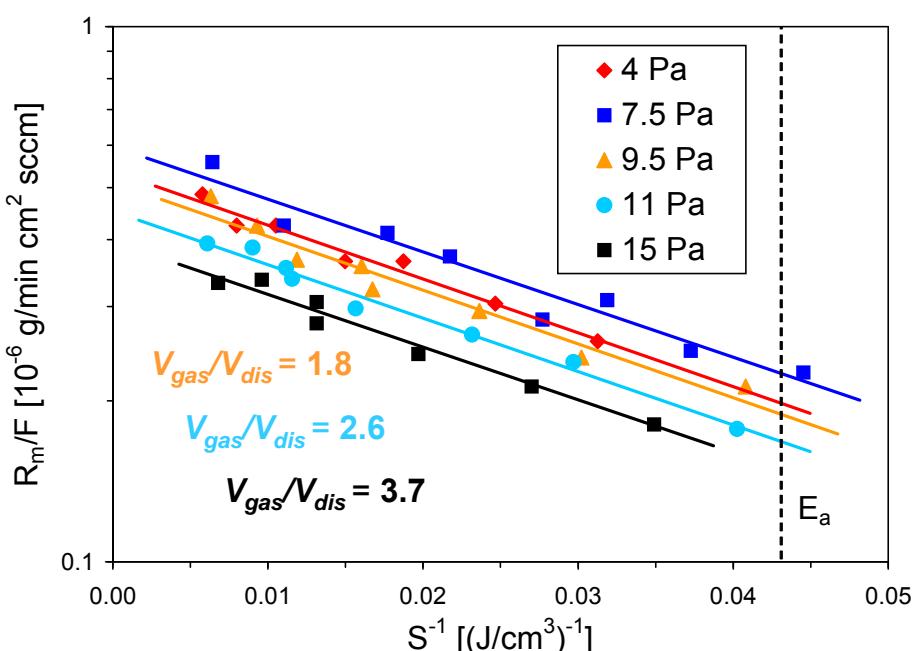
$$S = \frac{W}{F} \frac{d_{act}}{d_{gas}} \frac{V_{gas}}{V_{dis}}$$

$V_{gas} > V_{dis}$   
corner-dominated

Transition from volume- to corner-dominated discharge at a pressure >8 Pa.

# Influence of Pressure

## Consideration of similarity factor

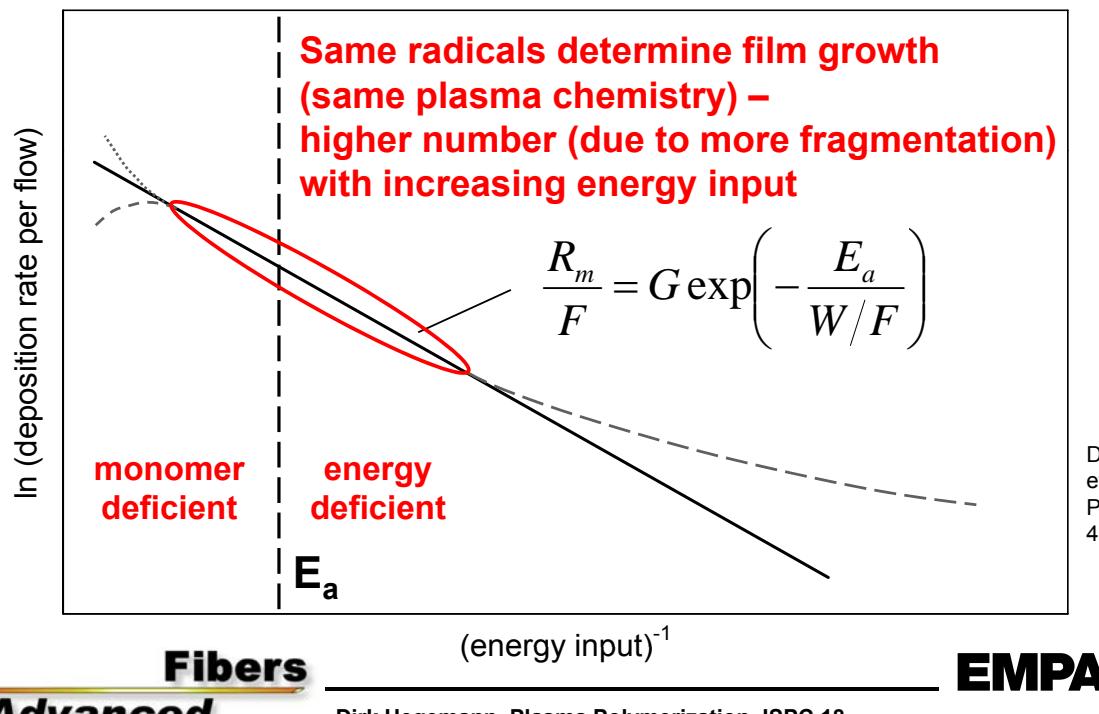


$$S = \frac{W}{F} \frac{d_{act}}{d_{gas}} \frac{V_{gas}}{V_{dis}}$$

Introduction of similarity factor with decreasing discharge volume yield same activation energy.

# Plasma Polymerization

## Formation of film-forming radicals

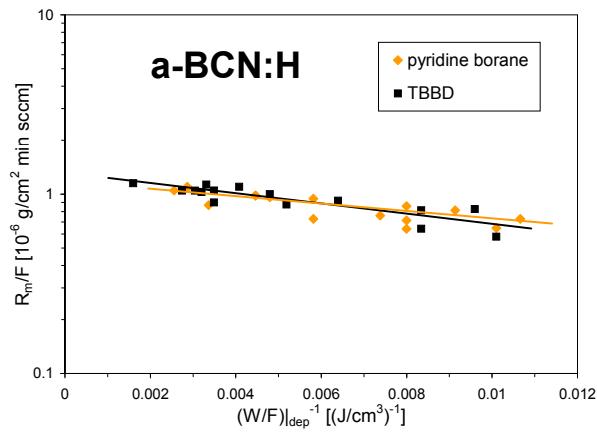
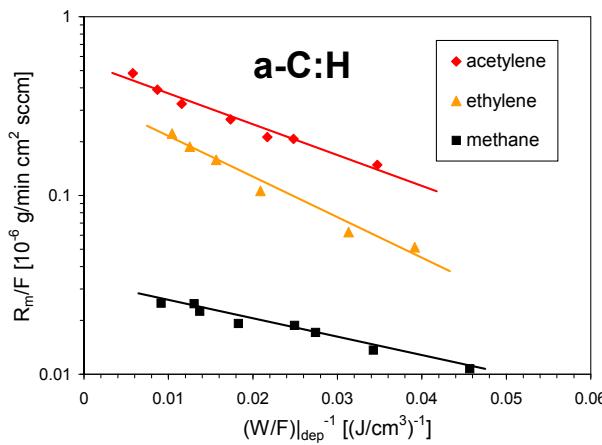


## Influence of Monomers

### Generalized activation energy

similarity factor enables the finding of a generalized activation energy

$$S = \frac{W}{F} \frac{d_{act}}{d_{gas}} \frac{V_{gas}}{V_{dis}}$$



# Influence of Monomers

## Generalized activation energy of different monomers

Monomer	Formula	Activation energy	Main dissociation
methane	CH <sub>4</sub>	5.3 ± 0.5 eV	C-H, (H-H)
acetylene	C <sub>2</sub> H <sub>2</sub>	9.0 ± 0.7 eV	C≡C
ethylene	C <sub>2</sub> H <sub>4</sub>	12 ± 1.2 eV	C=C, C-H (2x)
pyridine borane		12 ± 1.5 eV	C-N, C-C, N:B, C-H
TBBD		15 ± 1.5 eV	C-N (3x), C-C, C-H
HMDSO	(CH <sub>3</sub> ) <sub>3</sub> -Si-O-Si-(CH <sub>3</sub> ) <sub>3</sub>	12.8 ± 0.7 eV	Si-C, C-H, Si-O

## HMDSO Discharge

### Initiation of HMDSO plasma polymerization

$$E_a = 55 \text{ J/cm}^3$$

$$= 7.6 \text{ MJ/kg}$$

$$= 1230 \text{ kJ/mol (HMDSO)}$$

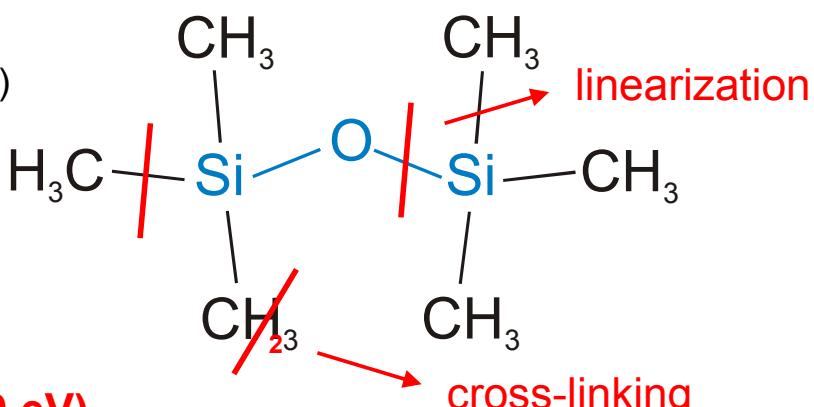
$$= 12.8 \text{ eV per molecule}$$

Si-O bond: 452 kJ/mol

Si-C bond: 360 kJ/mol

C-H bond: 435 kJ/mol

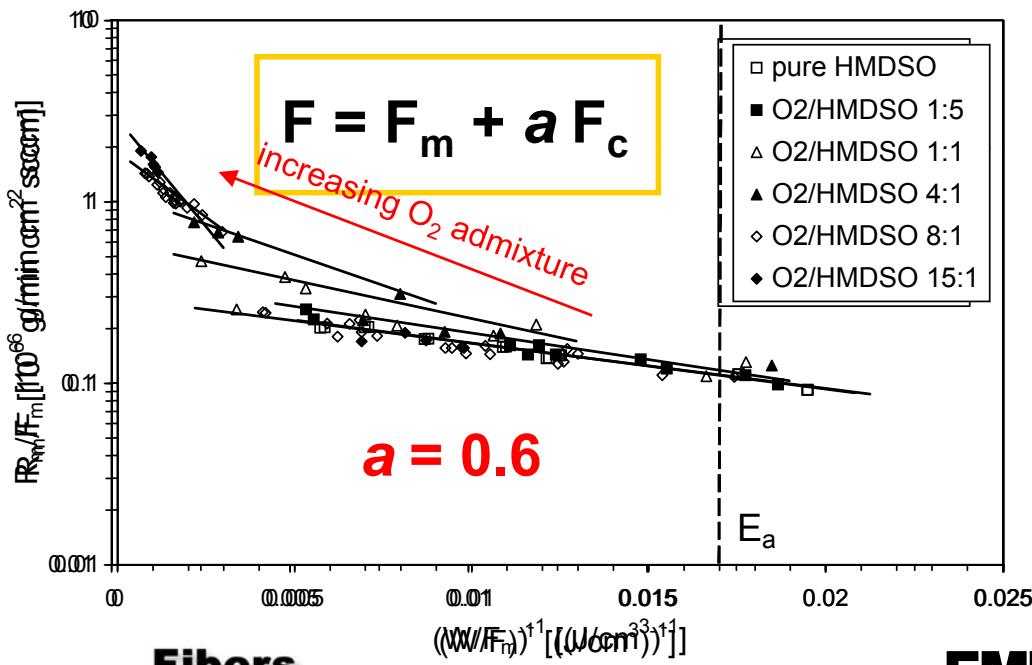
→ 1247 kJ/mol (12.9 eV)



The activation energy gives the dissociation energy to obtain the radicals that predominantly lead to plasma polymer growth.

# Influence of Carrier / Reactive Gases

## Oxygen added to HMDSO discharge



a: reaction crosssection  
→ energy consumed by carrier gas

D. Hegemann,  
M.M. Hossain,  
Plasma Process.  
Polym. 2005, 2,  
554.

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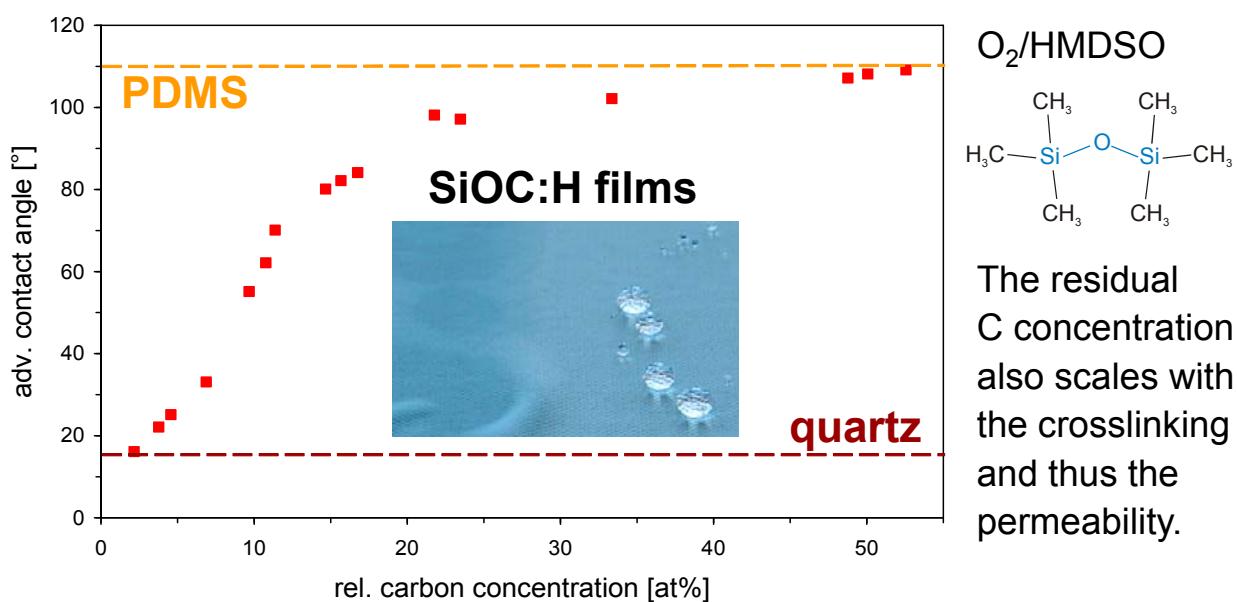
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# Design of O<sub>2</sub>/HMDSO Coatings

## Control of wetting properties



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# Influence of Carrier / Reactive Gases

Correction factor for the combined flow  $F = F_m + a F_c$

Monomer	Added gas	Flow factor a
hydrocarbons	Ar, He	0.05-0.1
	H <sub>2</sub>	~0.15
	CO <sub>2</sub>	~0.15
	N <sub>2</sub>	0.35
	NH <sub>3</sub>	0.5
HMDSO	O <sub>2</sub>	0.6
Acrylic acid	H <sub>2</sub>	~0.25

D. Hegemann  
et al., Plasma  
Process. Polym.  
4, 2007, 229.

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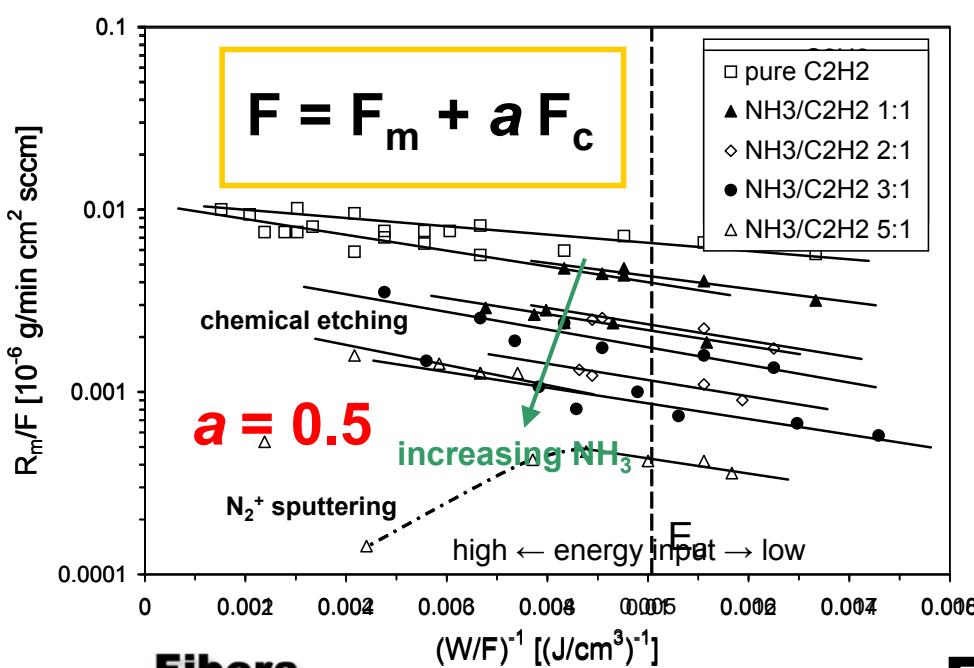
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# Influence of Reactive Gases

Plasma polymerization of hydrocarbon/ammonia



a: reaction  
crossection  
→ energy  
consumed  
by carrier  
gas

D. Hegemann,  
M.M. Hossain,  
Plasma Process.  
Polym. 2005, 2,  
554.

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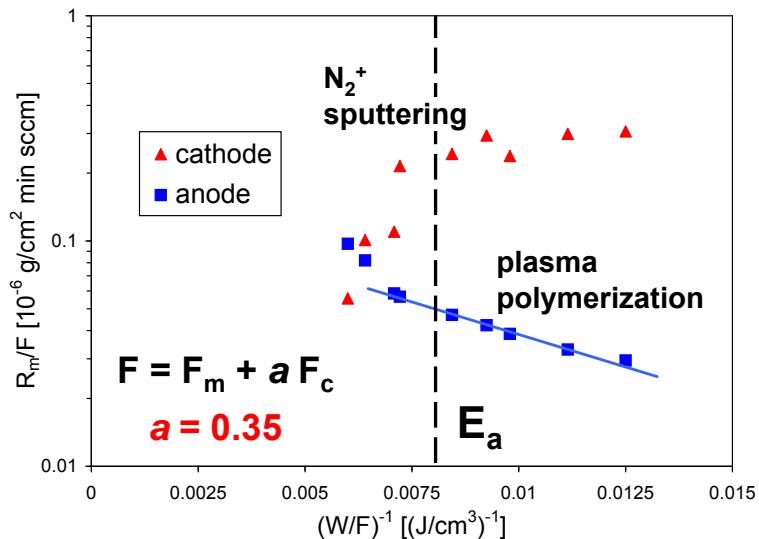
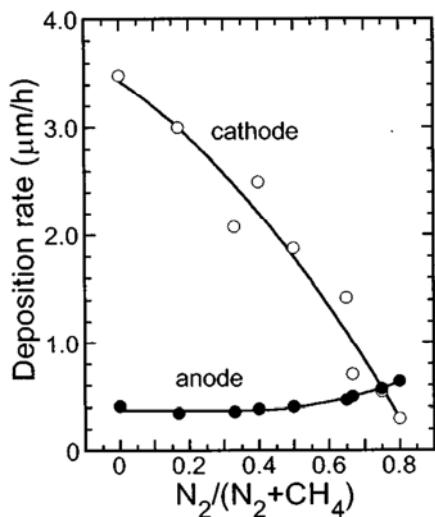


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# Re-Engineering

## Plasma polymerization of asymmetric N<sub>2</sub>/CH<sub>4</sub> discharges

RF plasma, 40 Pa, -650 V<sub>bias</sub>



M. Zhang, Y. Nakayama, T. Miyazaki, M. Kume, J. Appl. Phys. 85, 1999, 2904.

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Dirk Hegemann, Plasma Polymerization, ISPC 18

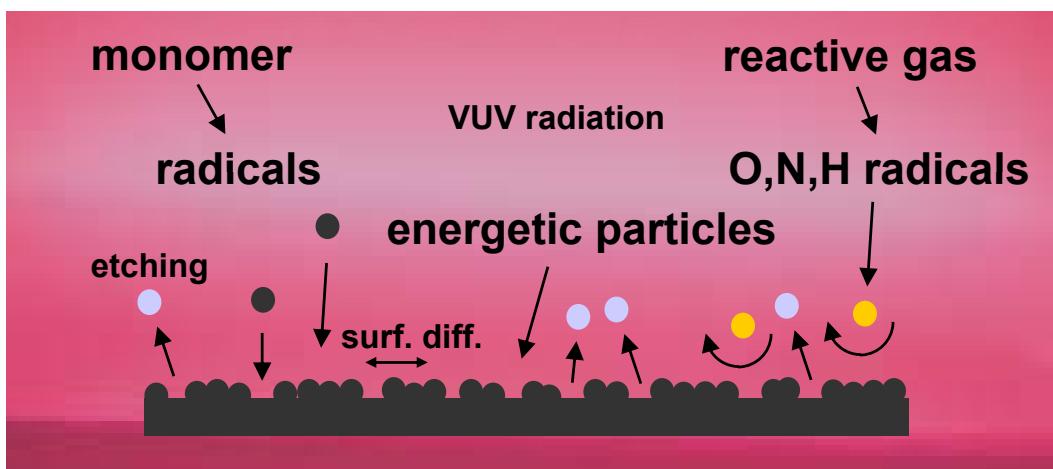
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## Deposition of Nanoporous Coatings

### Rivaling deposition/etching processes

plasma polymerization + chem./phys. etching



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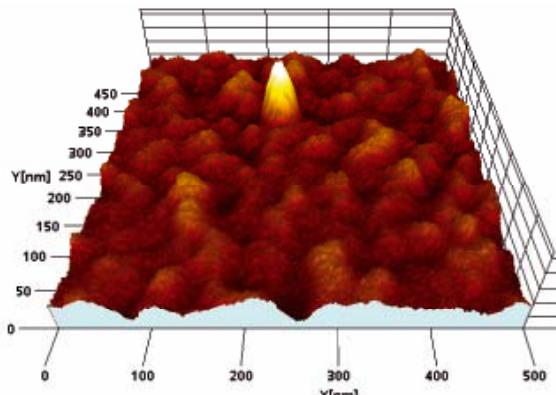
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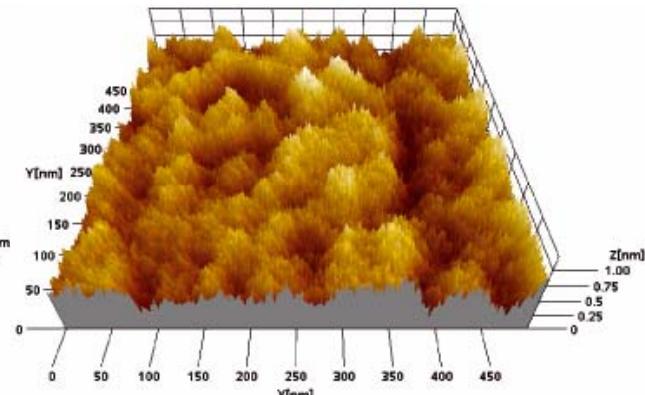
# Deposition of Nanoporous Coatings

## Hydrocarbon/ammonia RF discharges

Amine-functionalized coatings



porous structure: <30 nm



porous structure: <20 nm

D. Hegemann, M.M. Hossain, D.J. Balazs, Prog. Organic Coat. 58, 2007, 237.

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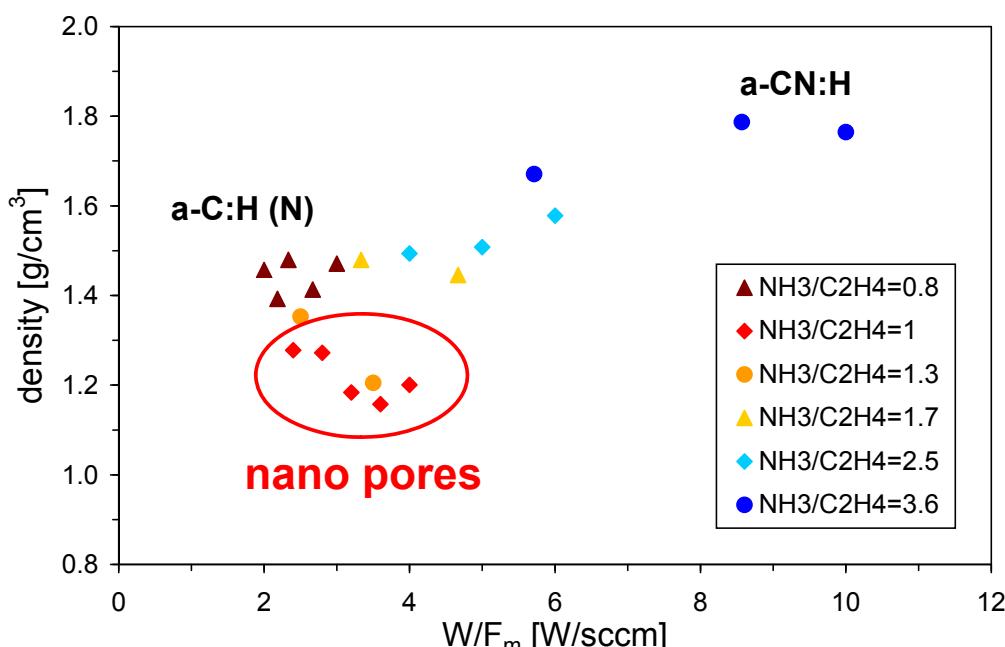
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# Deposition of Nanoporous Coatings

## Film density related to porous structure



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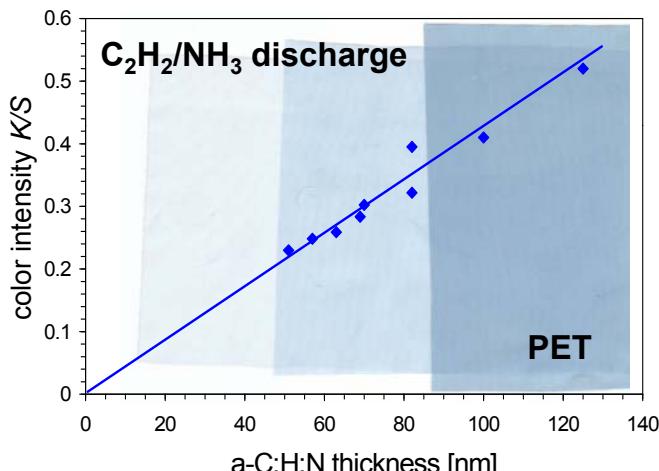
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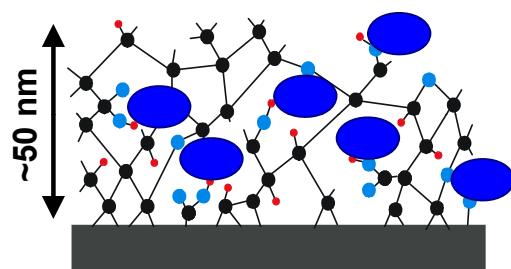
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# Nanoporous Plasma Coatings

## Dyeing of plasma coatings on textile fabrics



dyestuff: C.I. Acid blue 127:1



Dye molecules (~3 nm)  
are able to diffuse into  
nanoporous structure.

M.M. Hossain, A.S. Herrmann, D. Hegemann, Plasma Process. Polym. 4, 2007, 135.

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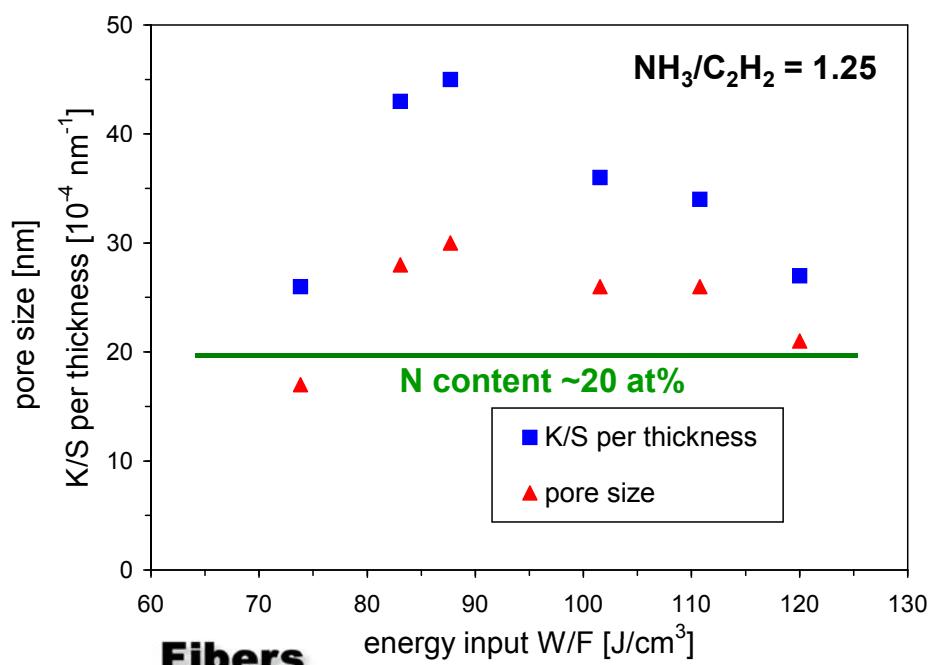
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# Nanoporous Plasma Coatings

## Dyeability (color intensity K/S) vs. pore sizes



Color intensity  
correlates with  
pore sizes,  
while overall  
N content is  
constant for a  
fixed NH<sub>3</sub>/C<sub>2</sub>H<sub>2</sub>  
ratio.

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# Nanoporous Plasma Coatings

## Permanence of dyed plasma coatings on textile fabrics

Martindale before testing

PP  
multifil



after 70'000 cycles



PET  
monofil



dyestuff: C.I.  
Acid blue 127:1

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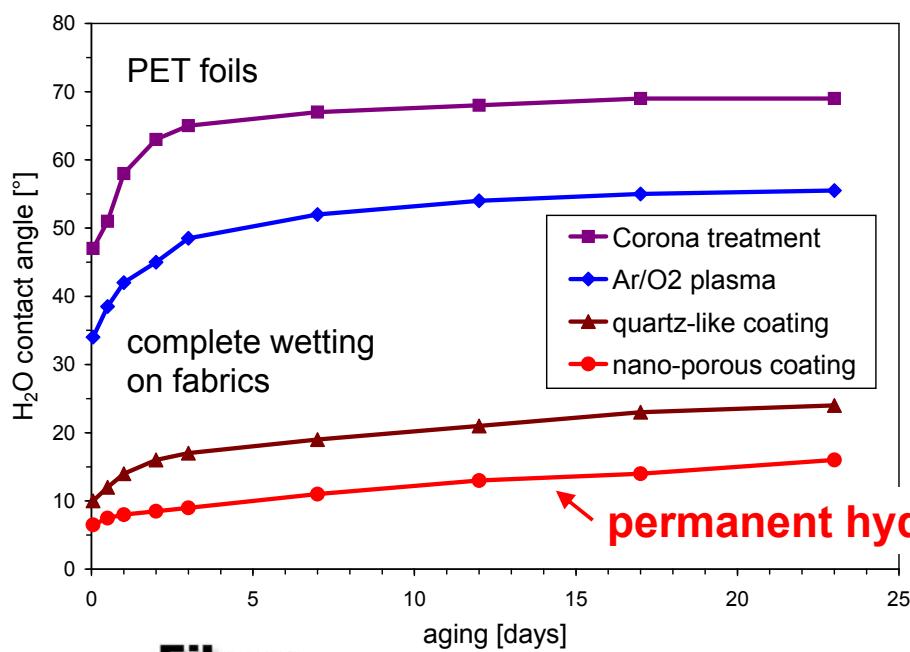
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# Nanoporous Plasma Coatings

## Hydrophilic treatment – hydrophobic recovery



Aging due to internal and external effects:  
- re-organization  
- surface reactions  
- absorption layers

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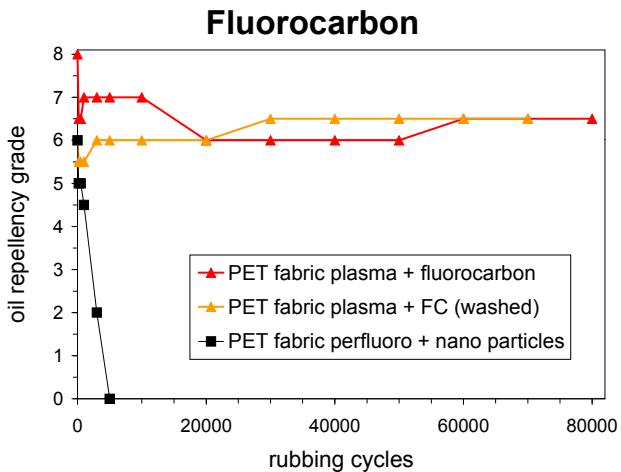
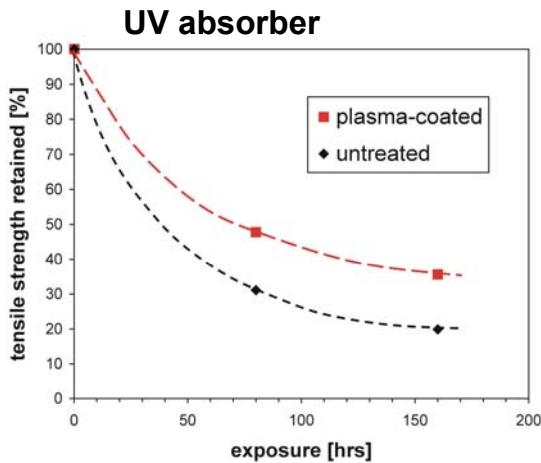
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# Nanoporous Plasma Coatings

## Loading with wet chemicals



UV exposure  
of aramid fabrics



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Martindale  
abrasion test



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## Transfer of Plasma Polymerization

### Scale-up to Web Coater

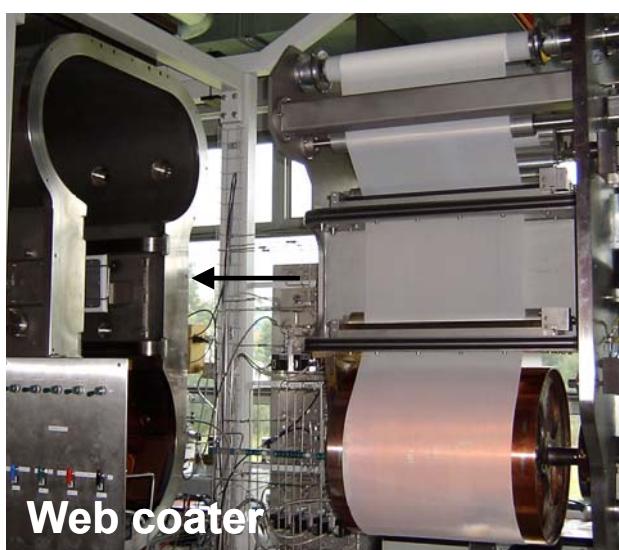


Continuous processing of  
textiles, membranes, foils,  
bands, and papers

width = 65 cm

velocity = 0.1..100 m/min

$A_{dep} = 10'000 \text{ cm}^2$



**Web coater**

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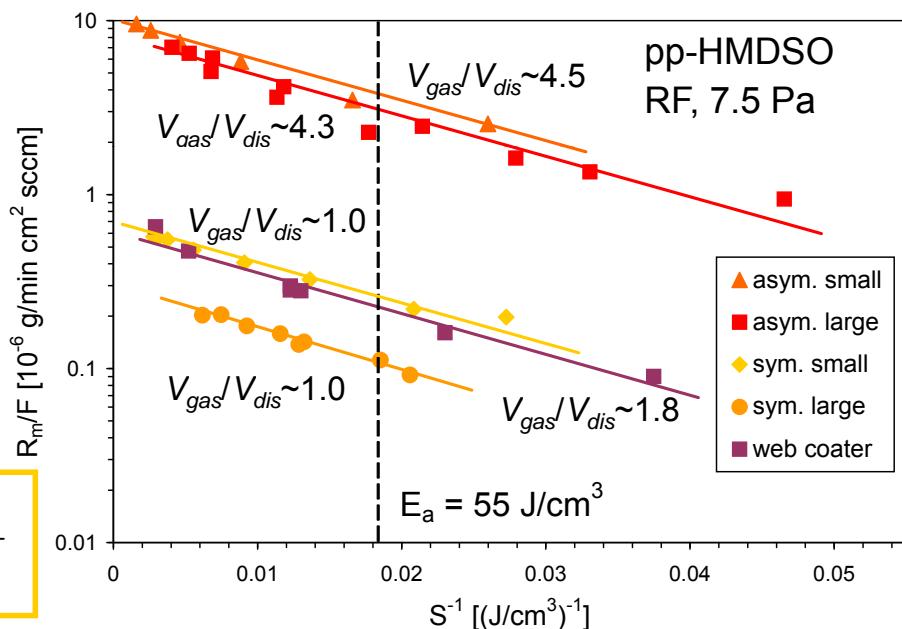
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# Transfer of Plasma Polymerization

## Different reactor geometries

Scale-up can be performed successfully using the identified similarity parameter

$$S = \frac{W}{F} \frac{d_{act}}{d_{gas}} \frac{V_{gas}}{V_{dis}}$$



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**Advanced**

Dirk Hegemann, Plasma Polymerization, ISPC 18



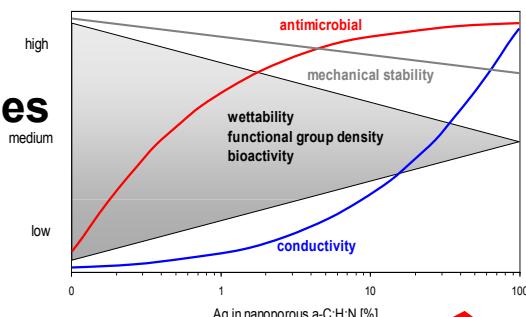
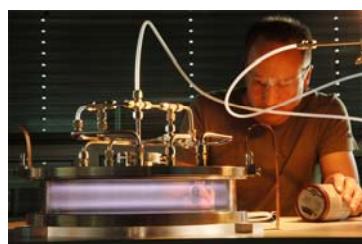
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## Outlook

### Control of Plasma Polymerization Processes

#### control / design of

- plasma reactors
- nano-scaled coatings
- nanoporous coatings
- multifunctional (textile) surfaces
- transfer into industry



**Fibers**  
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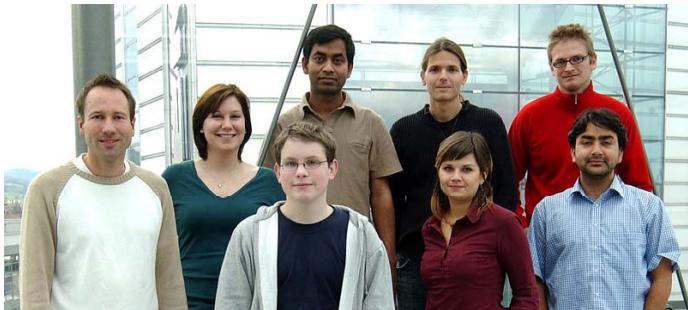


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# Acknowledgement

## Laboratory of Advanced Fibers

### ■ Plasma group



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■ CTI Bern (funding) **KTI/CTI**

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