# Bi-reforming with a ratio of $CH_4/CO_2/H_2O = 3/1/2$ by plasma catalysis for power to fuels

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**Abstract:** Bi-reforming of CH<sub>4</sub> in plasma catalytic reforming (PCR) was studied, aiming on directly produce high-quality syngas with an ideal H<sub>2</sub>/CO = 2. PCR was composed of a gliding arc plasma and a tubular catalytic reactor with Ni/CeO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> packing. Results shown that CO<sub>2</sub> conversion is more favourable than H<sub>2</sub>O conversion in warm plasma, on the contrary, H<sub>2</sub>O conversion is more favourable over catalysts. Therefore, bi-reforming of CH<sub>4</sub> can be really achieved with a stoichiometric ratio of CH<sub>4</sub>/CO<sub>2</sub>/H<sub>2</sub>O = 3/1/2. And then high-quality syngas with H<sub>2</sub>/CO=2 is obtained at an energy efficiency of 65% and near conversions of 65±1% for CH<sub>4</sub>, CO<sub>2</sub> and H<sub>2</sub>O.

Keywords: Plasma reforming, Plasma catalysis, CH<sub>4</sub> conversion, CO<sub>2</sub> conversion.

#### 1. Introduction

Bi-reforming of CH<sub>4</sub>,

 $3CH_4 + CO_2 + 2H_2O \rightarrow 4CO + 8H_2$  (R1) is a promising process can directly produce high quality syngas with an ideal H<sub>2</sub>/CO = 2. This process has been studied by conventional catalytic method. However, it is found that H<sub>2</sub>O conversion is much favourable than CO<sub>2</sub> conversion, resulting this process can't be realized at the stoichiometric ratio of R1. In addition, the strong endothermic feature of R1 is also one of the challenge for conventional method.

In plasmas, electron can be accelerated selectively and obtains almost all the plasma energy to form a non-thermal equilibrium to induce reaction at a mild condition. Up to now, various plasma types have been studied for chemical processes. Amongst those plasmas, warm plasma formed by gliding arc (GA) has been believed to be one of the most promising plasma types, because it operates at atmospheric pressure, and exhibits a high energy efficiency. Especially, the vibrational excitation of CO<sub>2</sub> in GA plasma results the efficient dissociation of CO2. Moreover, plasma is commonly generated by electric power and can be quickly switched on/off. Hence, it is feasible to power plasma with the fluctuant solar electricity and store it to fuels. In Laboratory of Plasma Physical Chemistry (LPPC), Dalian University of Technology, we have developed an efficient reactor and technique of plasma catalytic reforming (PCR) by combining GA plasma with catalysts <sup>1, 2, 3</sup>. In this work, we studied bi-reforming of CH4 in PCR. The really bireforming of CH<sub>4</sub> reacting at its stoichiometric ratio is achieved, because PCR supplies activation for both of CO<sub>2</sub> and H<sub>2</sub>O. Moreover, high-quality syngas with H<sub>2</sub>/CO=2 is obtained at an energy efficiency of 65%.

#### 2. Experimental

Fig. 1 shows a schematic diagram of the PCR reactor developed at LPPC. The numbers 1, 2, 3, 4, 5, 6, 7, 8, represent the high-voltage electrode, ceramic insulator, plasma zone, catalyst bed zone, heater, two movable thermocouples for recording the temperature of the catalyst bed and the reactor wall (6 for TCB and 7 for TRW), and a static thermocouple (8 for TH) located at the half-height of



Fig. 1 Schematic diagram of the PCR reactor

the heater. To avoid carbon deposition in plasma reactor, the reactants are fed from two inlets. One flow (F1), which is a mixture of CH<sub>4</sub>/CO<sub>2</sub>/H<sub>2</sub>O = 3/x/6-x,  $0 \le x \le 6$ , is used to form vortex flow in GA reactor with a flow rate of 2.2 SLM. The other flow (F2), which is pure CH<sub>4</sub> with flow rate of 0.7 SLM, is fed after GA reactor but before catalyst bed to adjust the total molar ratio of  $CH_4/CO_2/H_2O = 6/x/6$ x (x = 2 is the reaction molar ratio for bi-reforming). A DChigh-voltage power source is connected to the high-voltage electrode, to generate a GA discharge at atmospheric pressure. The discharge voltage, current and power are recorded by an oscilloscope (DPO 4104B, Tektronix) via a voltage probe (P6015A, Tektronix) and a sampling resistor  $(51\Omega)$ , respectively. A spectrograph (Shamrock SR-750, Andor) with an ICCD detector (iStar DH734, Andor) was adopted to record optical emission spectra (OES) of GA plasma. The Ni/CeO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> catalysts with weight of 10 g, containing Ni of 11 wt.% and Ce of 8 wt.%, are packed in the post-plasma zone. A home-made heater is employed for additional heating of the catalyst bed. The gaseous products are analyzed by two online gas chromatographs (Agilent 1790 and Agilent 6890 N) by using N<sub>2</sub> as internal standard of CO, CH<sub>4</sub>, CO<sub>2</sub> and hydrocarbons (C<sub>2</sub>H<sub>6</sub>, C<sub>2</sub>H<sub>4</sub> and C<sub>2</sub>H<sub>2</sub>), and helium as internal standard of H<sub>2</sub>.

#### 3. Results and discussion

The waveforms at F1 molar composition of CH<sub>4</sub>/CO<sub>2</sub>/H<sub>2</sub>O = 3/1/2 and discharge power of 180 W is illustrated in Fig. 2. It is shown that the GA discharge possesses the classic ignition-evolution-extinguishment with a period of ~1.6 ms. The arc channel is ignited at

voltage of ~3.5 kV. Once the arc ignited, the discharge voltage drops to ~2.6 kV at a current of ~69 mA, and then voltage and current increases and decreases gradually to extinguishment (re-ignition), respectively, with arc gliding. As the opposite trends of voltage and current, the discharge power fluctuates in  $180 \pm 6$  W.



Fig. 2 Waveforms of discharge voltage, current and power

Plasma parameters of GA plasma in a mixture of CH<sub>4</sub>/CO<sub>2</sub>/H<sub>2</sub>O were determined with OES in a wavelength range of 300 - 800 nm. Molecular spectra of OH, CH, CO and C2 were observed. In addition, atomic lines of  $H_{\alpha}$  and  $H_{\beta}$  from Balmer lines and oxygen triple lines at 777 nm from O atom were detected. Amongst those spectra, C2 Spectra was used to evaluate vibrational and rotational temperatures. By comparing the simulated and measured spectra of C2 as shown in Fig. 3, the vibrational and rotational temperatures can be estimated as 3900 K and 2500 K, respectively. The rotational temperature can be a measure for gas temperature in the arc channel, because they are in the thermal equilibrium. In addition, vibrational temperature is higher than rotational temperature. Obviously, this was attributed to the non-thermal equilibrium feature of GA plasma. Moreover, from Stark broadening of  $H_{\beta}$  deriving from its line profile (see Fig. 3b), the electron density was calculated as  $1.2 \times 10^{14}$  cm<sup>-3</sup>. Note that we also measured the plasma parameter at various molar ratios of CH<sub>4</sub>/CO<sub>2</sub>/H<sub>2</sub>O at SEI of 110 kJ/mol, results shown that the vibrational temperature, rotational temperature and electron density were insensitive with gas composition.

Fig. 4 presents the effect of  $CO_2/(CO_2+H_2O)$  molar ratio on reactant conversions and outlet temperature of GA reactor at discharge power of 180 W and F1 gas mixture of  $CH_4/CO_2/H_2O = 3/x/6-x$ . With increasing  $CO_2/(CO_2+H_2O)$ molar ratio from 0 to 1, conversions of  $CH_4$  and  $CO_2$ remained around 25% and 36%, respectively. However,  $H_2O$  conversion monotonously decreased with  $CO_2/(CO_2+H_2O)$  molar ratio. This implied that the warm plasma supplied a favorable condition for  $CO_2$  conversion, but not for  $H_2O$ . This should be attributed to the efficiently vibrational excitation of  $CO_2$  in warm plasma.



Fig. 3 Simulated and measured spectra of (a) C2 and (b)  $H_{\beta}$  at discharge power of 180 W and a gas mixture of CH<sub>4</sub>/CO<sub>2</sub>/H<sub>2</sub>O



Fig. 4 Effect of  $CO_2/(CO_2+H_2O)$  molar ratio on conversions and outlet temperature of GA reactor

Fig. 5 illustrated comparison of bi-reforming of CH<sub>4</sub> for plasma only (WP), conventional catalytic (CC) and plasma catalytic (WPC) cases at an overall molar ration of CH<sub>4</sub>/CO<sub>2</sub>/H<sub>2</sub>O = 3/1/2 and discharge power of 180 W and catalyst bed of 850 °C. Results clearly shown that CO<sub>2</sub> conversion is higher than H<sub>2</sub>O conversion in WP case, but it is lower than H<sub>2</sub>O conversion in CC. Therefore, in PCR case, similar conversions of CH<sub>4</sub>, CO<sub>2</sub> and H<sub>2</sub>O were achieved at around  $65 \pm 1\%$ . In addition, selectivities of H<sub>2</sub> and CO in CC and PCR cases were close to 100% due to effect of catalysis. The energy efficiency of bi-reforming of CH<sub>4</sub> in PCR was the highest amongst those three cases. Moreover, the ideal syngas with H<sub>2</sub>/CO=2 was obtained directly.



Fig. 5 Comparison of bi-reforming of CH4 for WP, CC and WPC cases

### 4. Conclusion

Bi-reforming of CH<sub>4</sub> in plasma catalytic reforming (PCR), composed of a GA plasma and Ni/CeO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> catalyst, was studied. Electron density, vibrational and rotational temperature in GA plasma was diagnosed as  $1.2 \times 10^{14}$  cm<sup>-3</sup>, 3900 K and 2500 K, which are typical parameter of warm plasma. Comparison of bi-reforming in WP, CC and WPC cases shown that, CO<sub>2</sub> conversion is higher than H<sub>2</sub>O conversion in WP case, but it is lower in CC case. Thus similar conversions of CH<sub>4</sub>, CO<sub>2</sub> and H2O are obtained in WPC case at reaction stoichiometric of bi-reforming of CH<sub>4</sub>. Consequently, high-quality syngas with an ideal H<sub>2</sub>/CO = 2 was achieved at an energy efficiency of 65% and near conversions of 65±1% for CH<sub>4</sub>, H<sub>2</sub>O and CO<sub>2</sub>.

## 5. Acknowledgements

This project is supported by the National Natural Science Foundation of China (11705019).

### 6. References

- [1] K. Li, J. L. Liu, X. S. Li, X. Zhu, A. M. Zhu, Chem. Eng. J. 288, 671(2016).
- [2] J. L. Liu, K. Li, X. S. Li, X. Zhu, A. M. Zhu, Catal. Today, 256, 96 (2015).
- [3] K. Li, J. L. Liu, X. S. Li, H. Y. Lian, X. Zhu, A. Bogaerts, A. M. Zhu, Chem. Eng. J. 353, 297 (2018).